



UNIVERSIDADE
FEDERAL DO CEARÁ



Laboratório de Pesquisa
em Adsorção e Captura de CO₂

ADSORPTION MICROCALORIMETRY AS A TOOL IN THE CHARACTERIZATION OF MESOPOROUS SILICAS FUNCTIONALIZED FOR CO₂ CAPTURE

Diana Azevedo



12º Encontro Brasileiro sobre Adsorção
23 a 25 de abril de 2018 | Gramado - RS

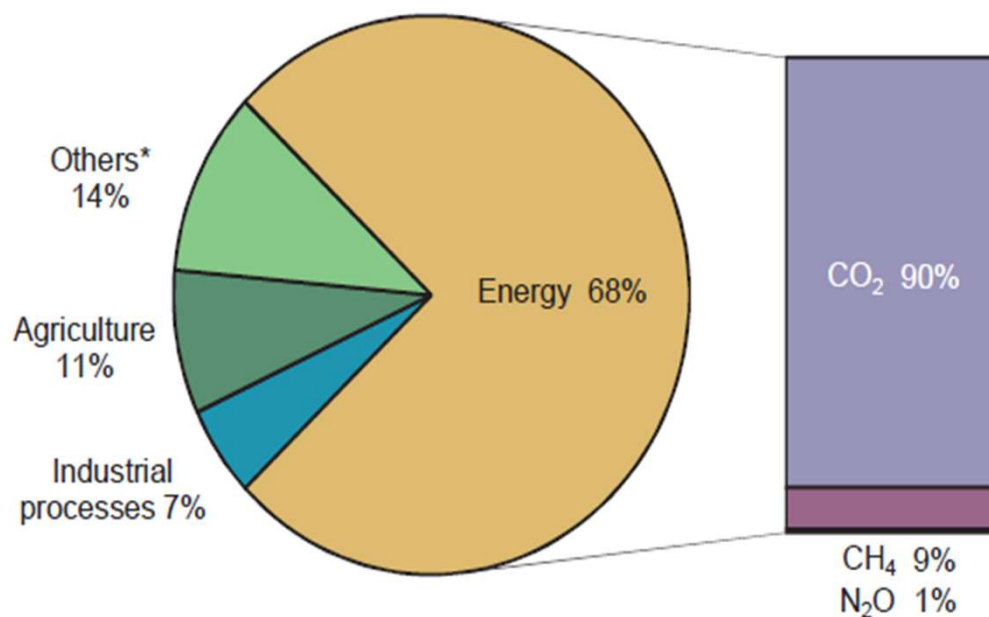


Fotografia de Leonid Streliaev



INTRODUCTION

- ✓ Climate changes/Greenhouse effect / GHG
- ✓ CO₂ is the second gas with the highest impact in radiation force
- ✓ CCS and CCUS technologies



Source: CO₂ Emissions from fuel combustion. Paris (IEA Statistical Review of world Energy, 2015).



INTRODUCTION

(Choi *et al*, 2009)

- What makes a good adsorbent? CO₂ adsorbent

adsorption/desorption
kinetics

CO₂ capacity

operating
window

Regenerability and
multicycle stability

Impact of common flue gas
components or
contaminants

- Commonly used adsorbents

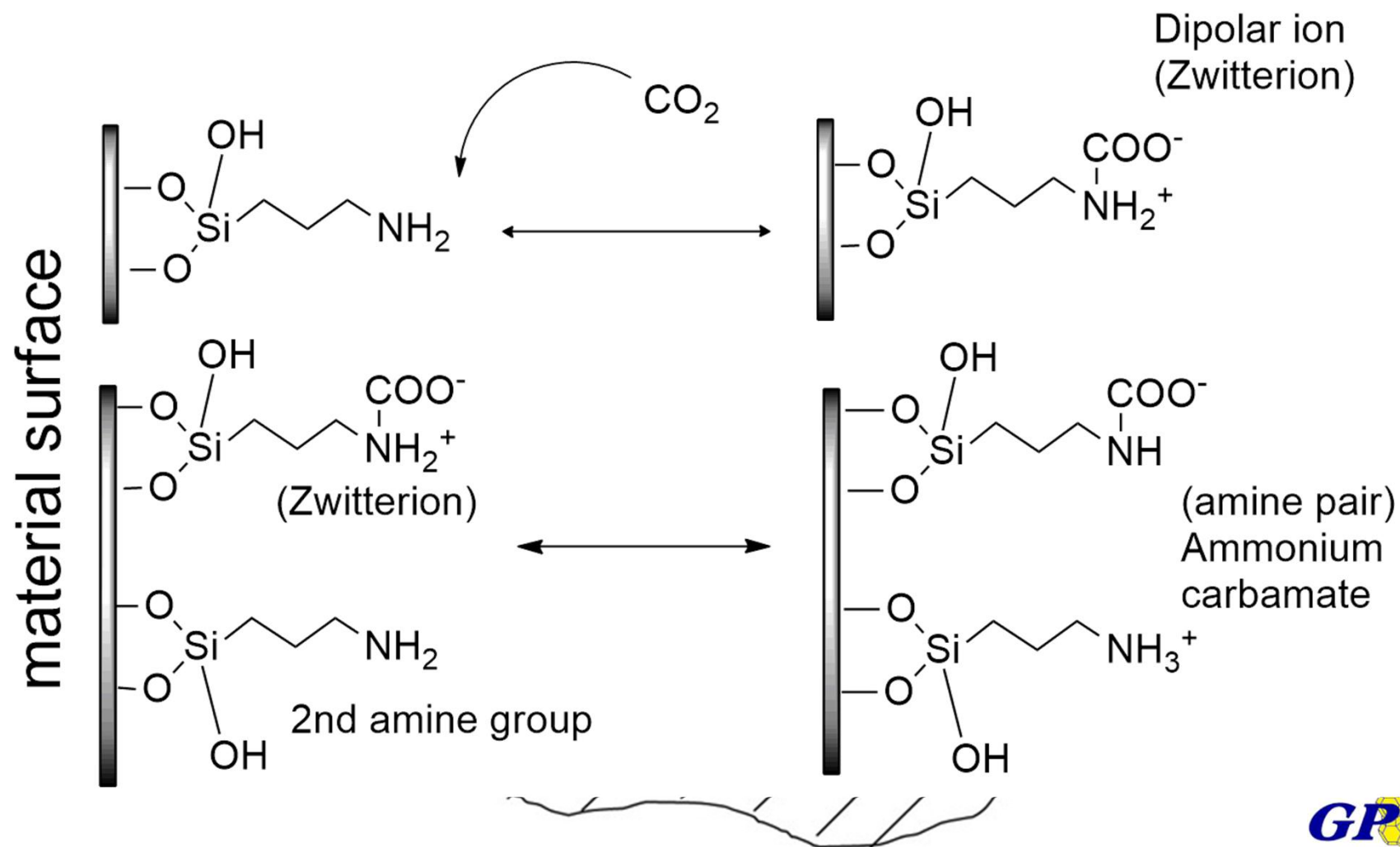
- Activated carbons
- Zeolites
- MOF'S
- Supported amines

Advantages:

- ✓ High CO₂ selectivity.
- ✓ Low susceptibility to temperature and water vapor
- ✓ Low degradation due to evaporation and vessel corrosion present in aqueous amine configurations.

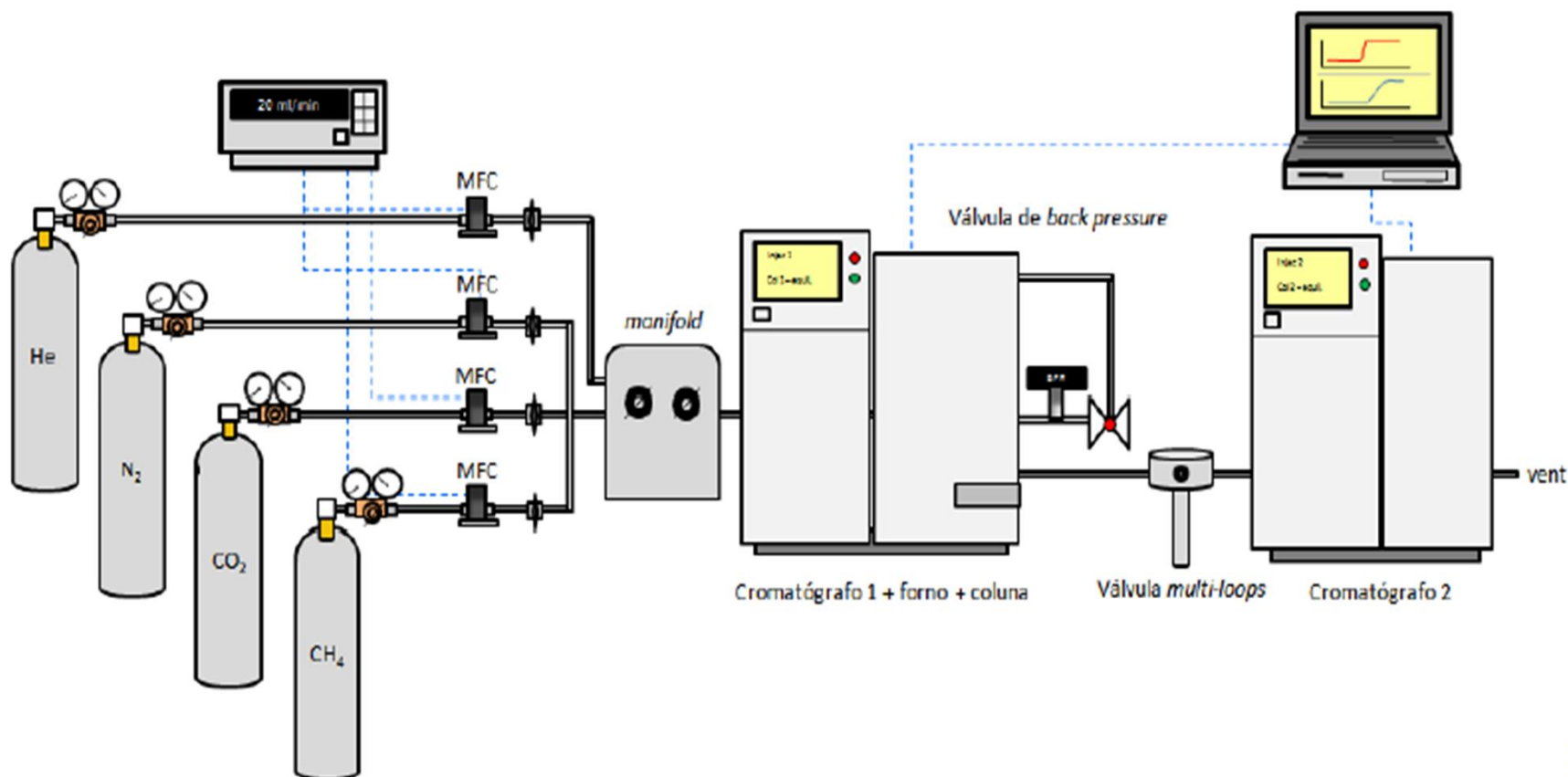
INTRODUCTION

Generally accepted interaction between CO₂ and primary amino group



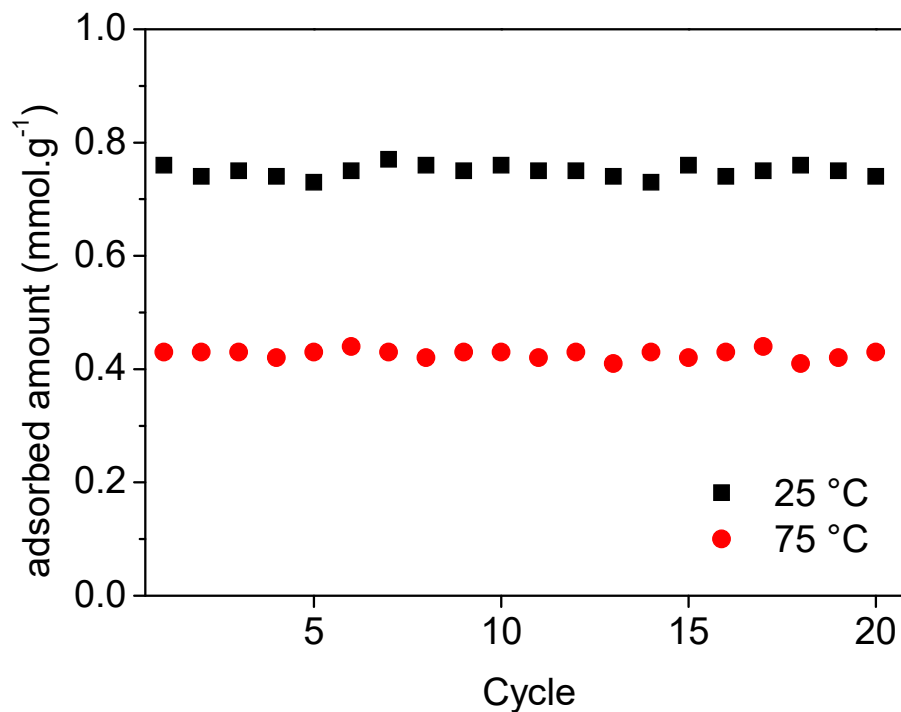
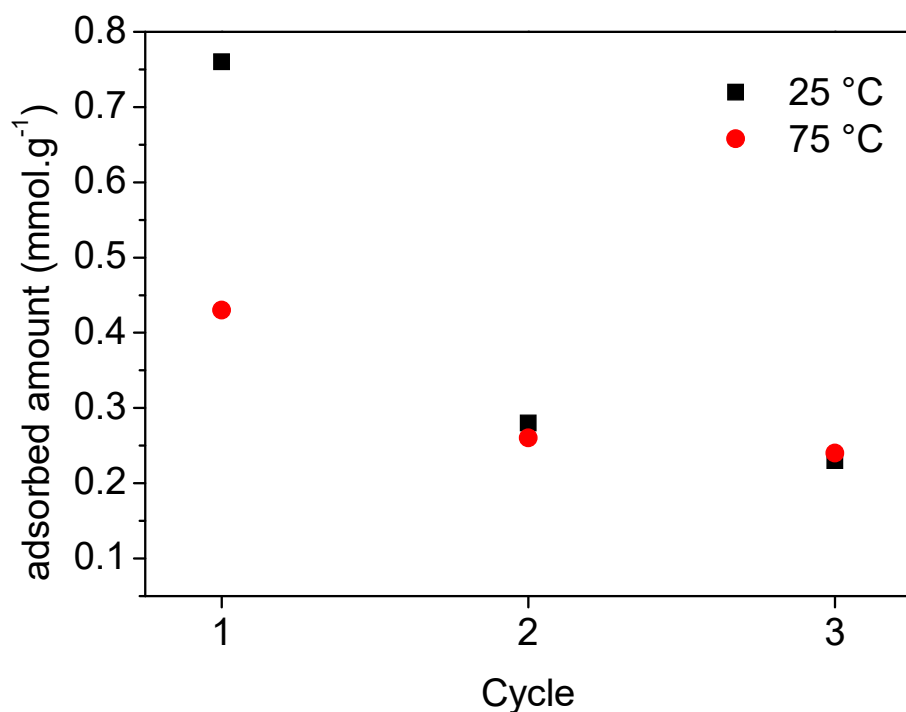
Previous experiments with amine-loaded silicas

(Santiago et al., submitted to J Envir Chem Eng, 2018)



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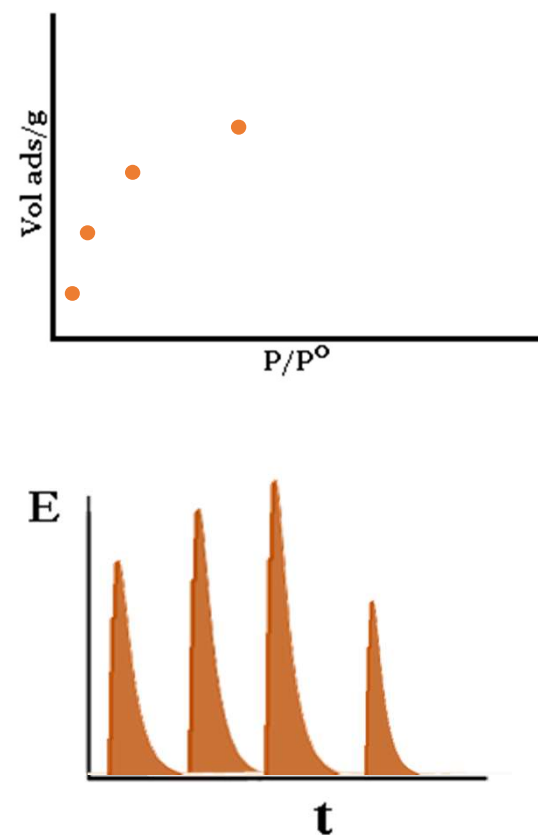
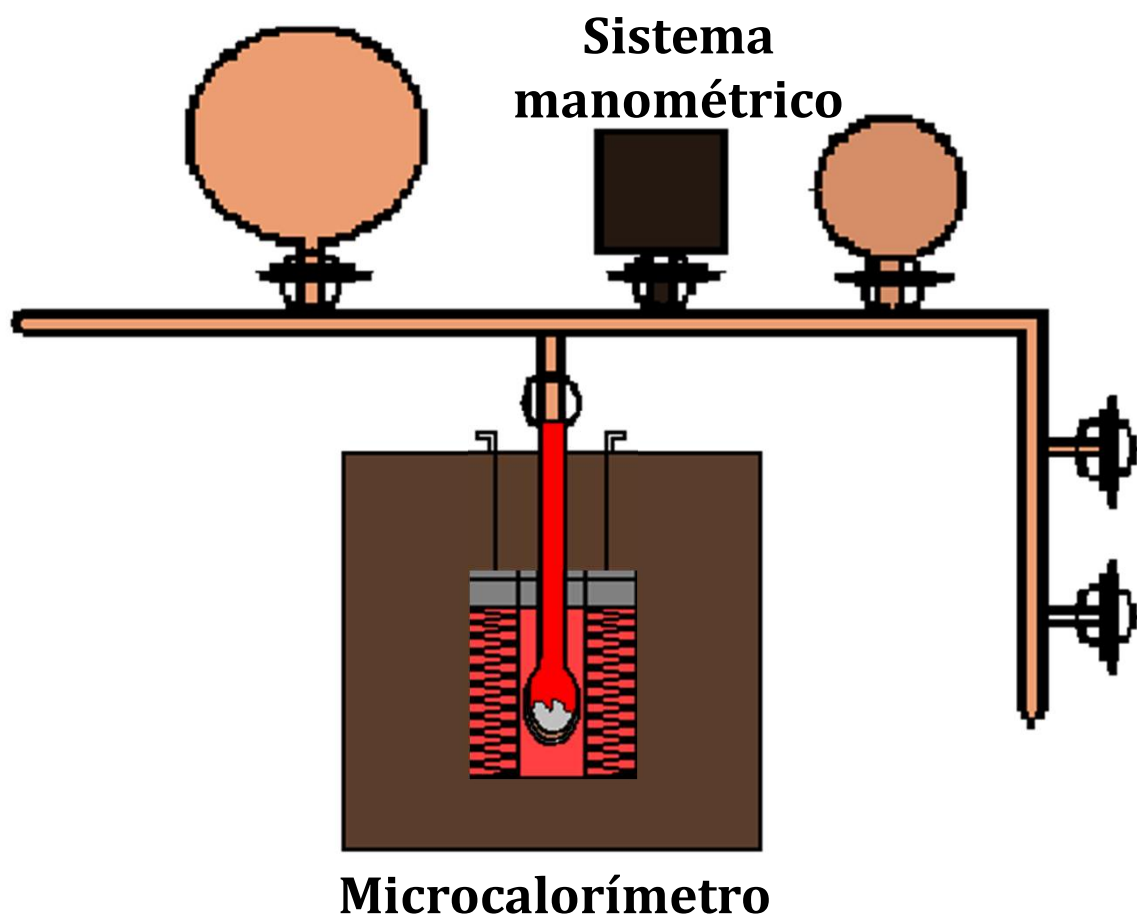
Questions???

- Is ammonium carbamate the only formed species in anhydrous conditions?
- Is physisorption also important? To which extent?
- How does the load of amine affect chemisorption products, reversibility, adsorption enthalpy and adsorbent stability?
- If several binding mechanisms occur, is there a rate-limiting step?

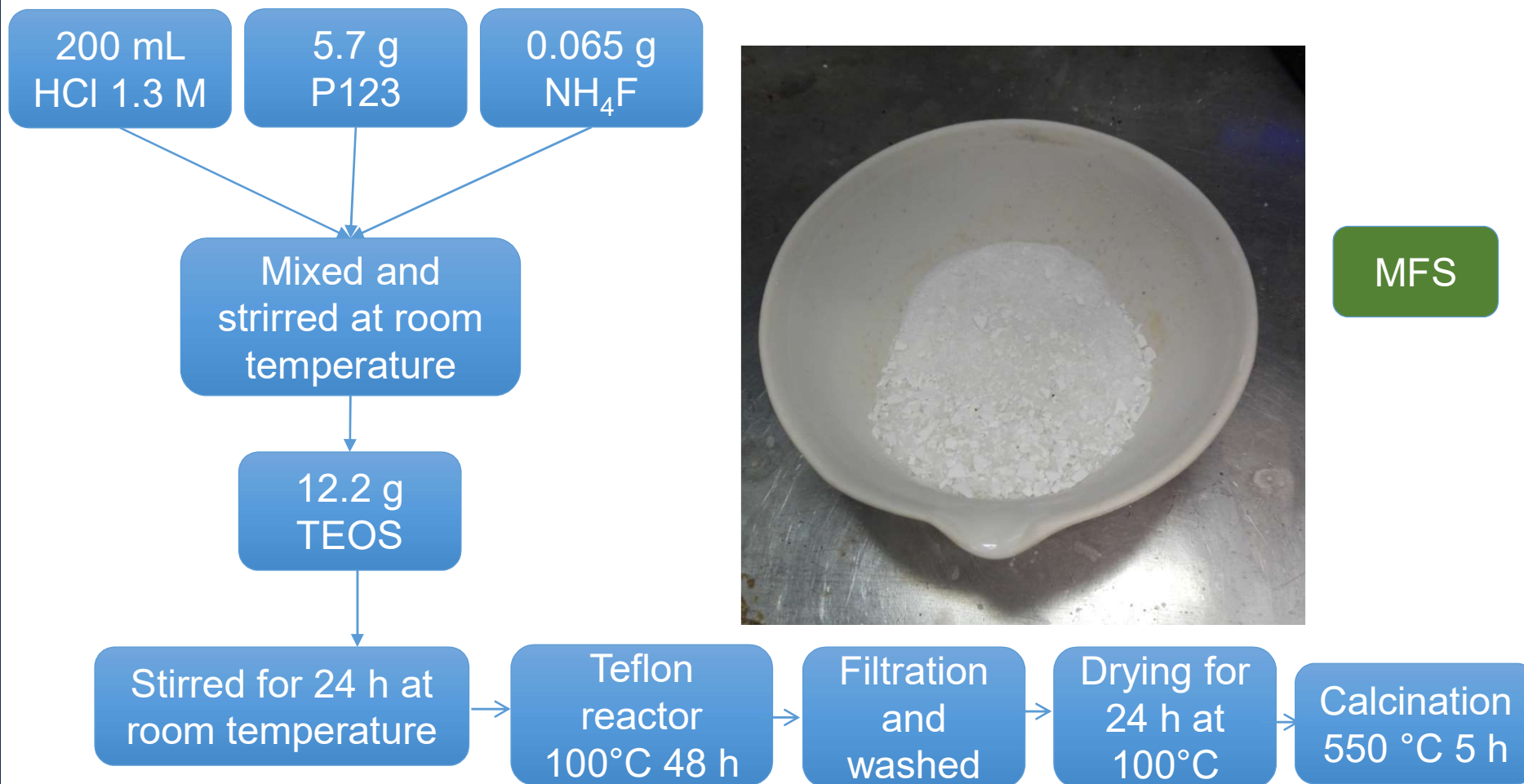
Differential microcalorimetry of adsorption – together with other characterization techniques – may provide insights into some of these questions!

Adsorption microcalorimetry

Soares-Maia, doctoral thesis, UNSL, 2014

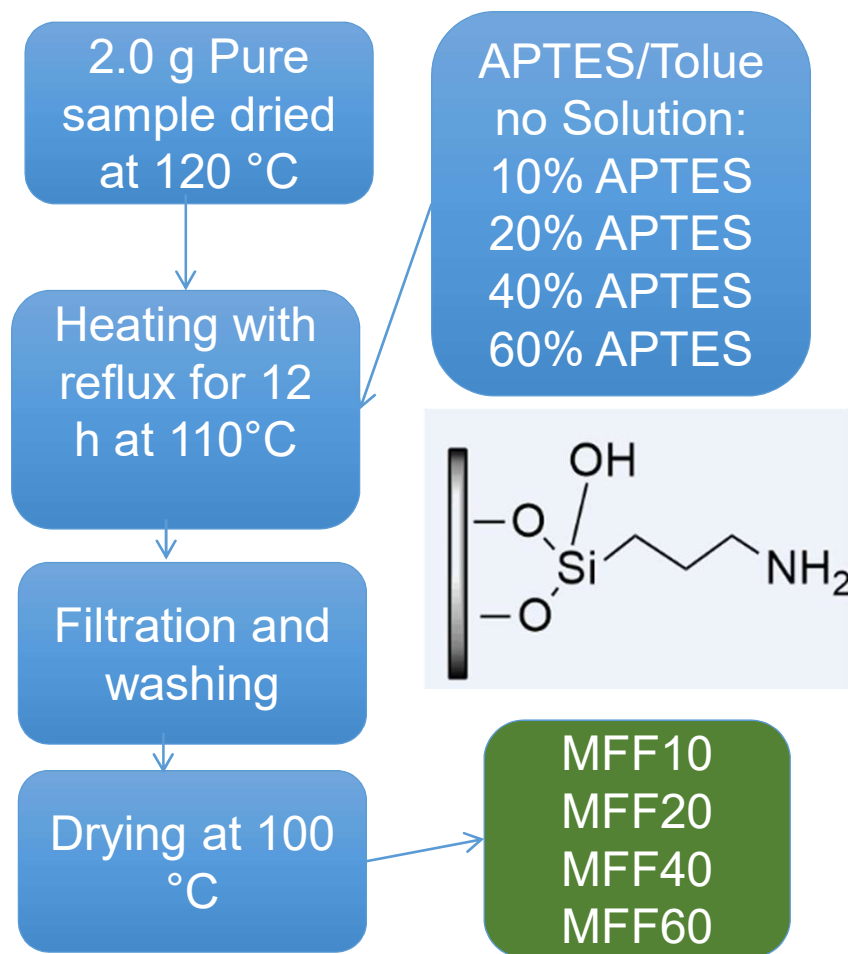


- Adsorbent / Pure Material Synthesis (Fulvio *et al*, 2005)



FULVIO, P., PIKUS, S. AND JARONIEC, M. *Journal of Materials Chemistry*, v.15, p. 5049 ;2005.

- Grafting (Hiyoshi *et al*, 2005)





EXPERIMENTAL - Methods

❖ Textural Characterization

➤ Nitrogen adsorption at -196 °C

- Specific Surface Area (BET Method)

$$A = n_m N_A \sigma_S$$

- Pore Volume

$$\hat{V}_{po} = n_{ads} \frac{M_{N_2}}{\rho_{N_2(l)}}$$

Autosorb-iQ3

- Micropore volume (DR method)

$$\hat{V}_{po(mic)} = n_{po(mic)} \frac{M_{N_2}}{\rho_{N_2(l)}}$$

- Pore size distribution (*BJH method*)

❖ Elemental Analysis

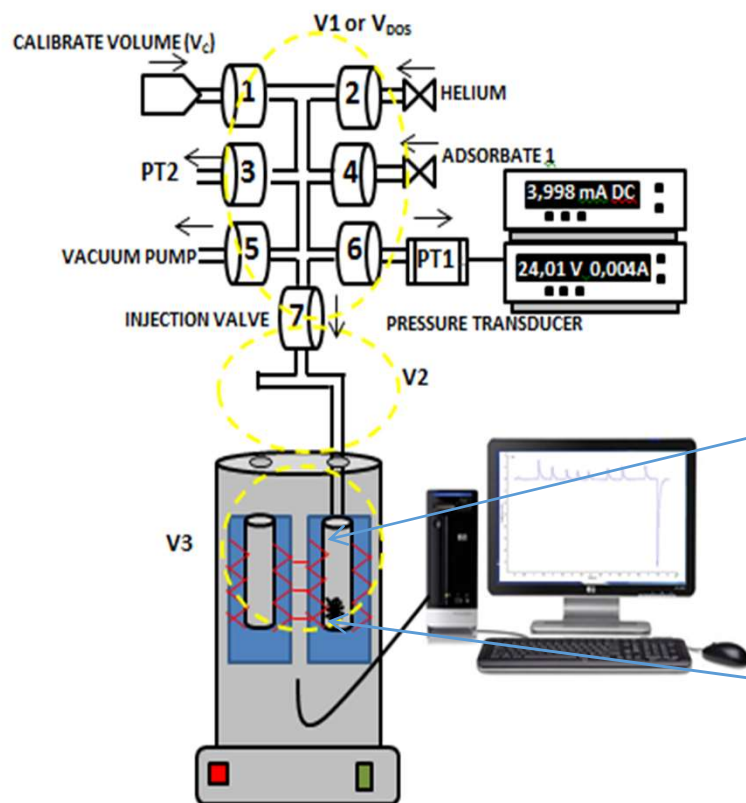
CHNS/O Analyzer 2400, Series II

❖ Nuclear magnetic resonance ²⁹Si NMR

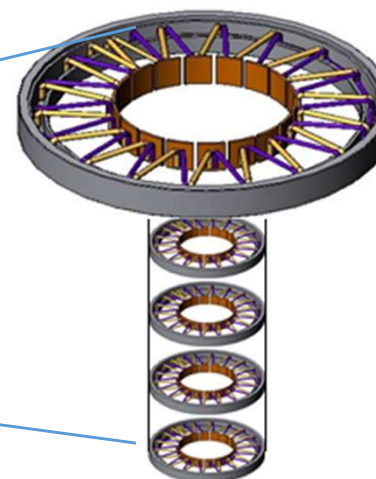
Bruker Avance II + 400

❖ Calorimetric experiments

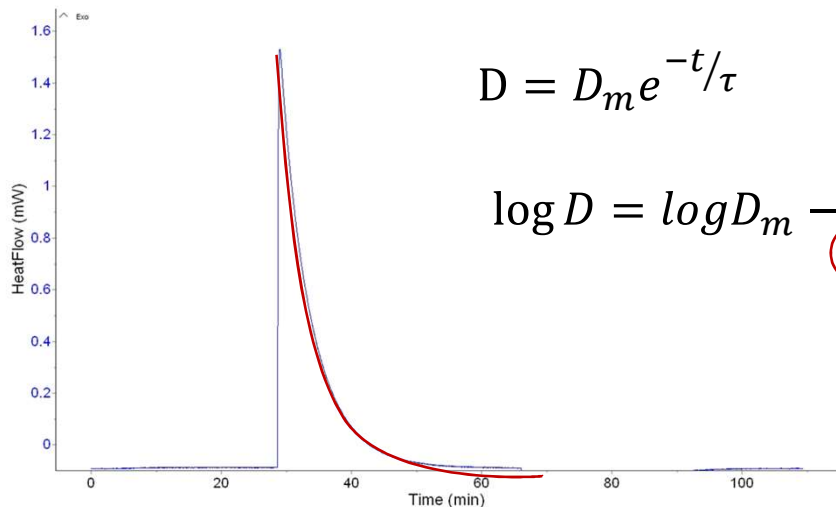
- Tian Calvet calorimeter Setaram C80



$$\Delta h_{ads,T,n} = \left(\frac{dQ_{rev}}{dn^\sigma} \right)_{T,A} + V_d \left(\frac{dp}{dn^\sigma} \right)_{T,A}$$

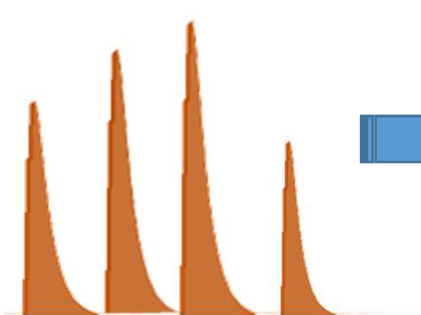
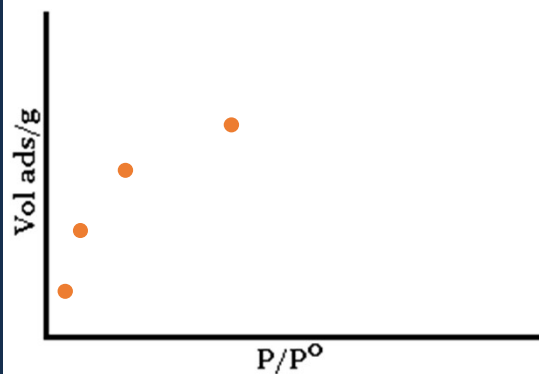


- Thermokinetic Parameter



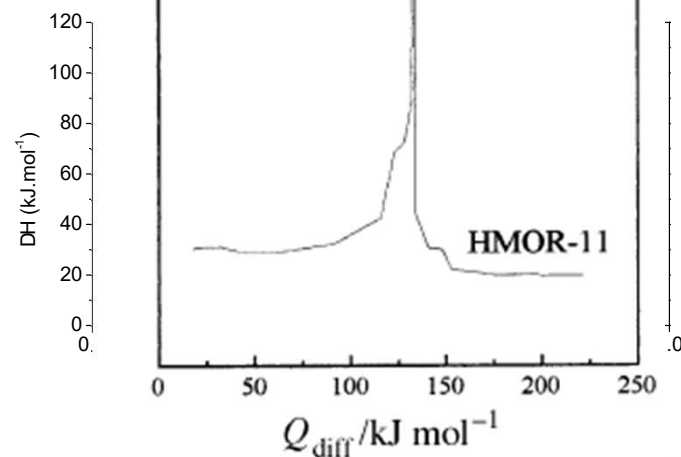
$$D = D_m e^{-t/\tau}$$

$$\log D = \log D_m - \frac{t}{\tau}$$



- Er

$$f(q) = -\frac{dn}{dp} \frac{dQ_{diff}}{dq}$$



$$\overline{in^{i-1}}$$

- Equilibrium Data (from manometric system of calorimeter)

$$n_{DOS} = \frac{p_i V_{DOS}}{RT_{DOS}}$$

$$n_e = \frac{p_{eq}(V_{DOS} + V_d)}{RT_{eq}}$$

$$n_i = \frac{p_{eq} V_d}{RT_{eq}}$$

$$n_{ads} = n_{DOS} + n_i - n_e$$

- Equilibrium Models

Duplo-Site Langmuir- Grafted samples

$$q_{CO_2} = \frac{q_{m,CO_2,1} \cdot b_1 P_1}{1 + b_1 P_1} + \frac{q_{m,CO_2,2} \cdot b_2 P_2}{1 + b_2 P_2}$$

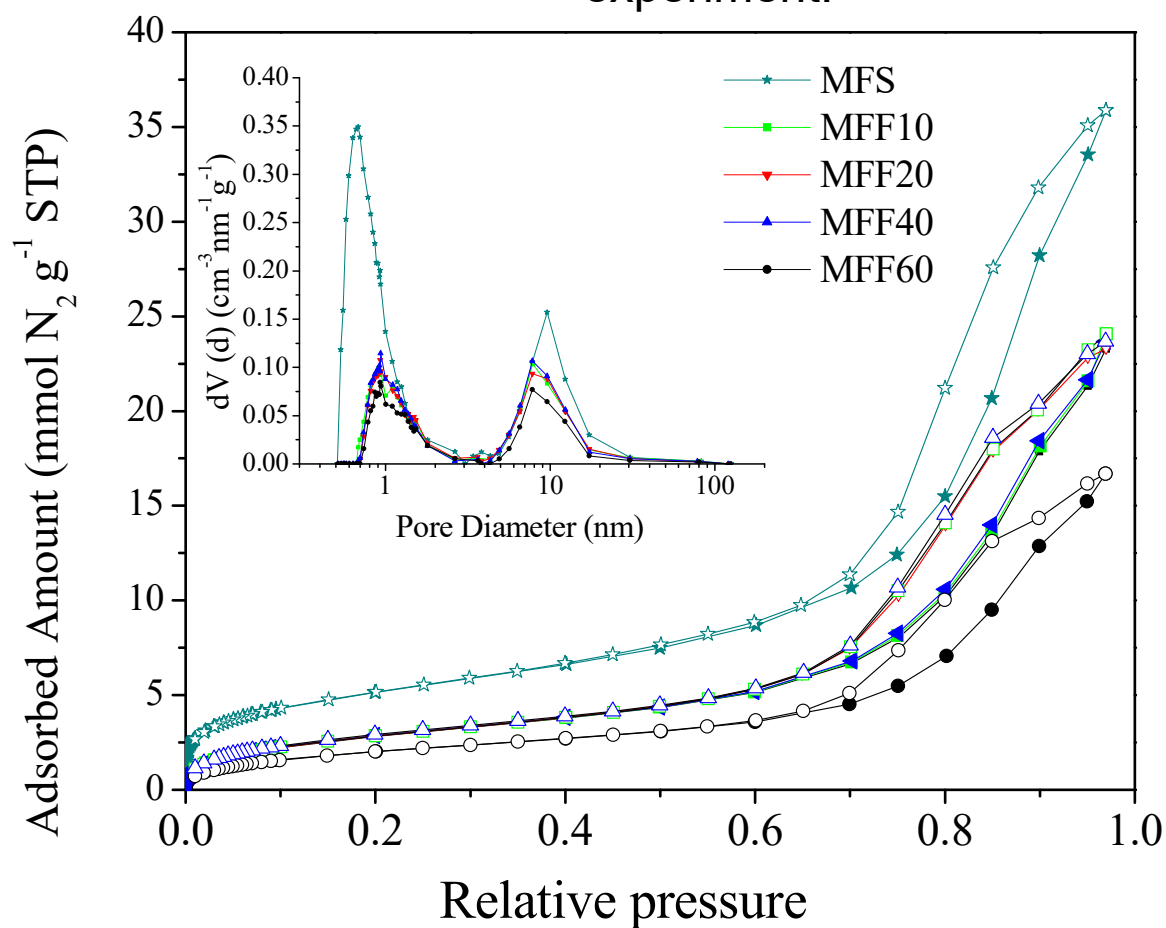
Langmuir- Pure sample

$$q_{CO_2} = \frac{q_m \cdot bp}{1 + bp}$$

❖ Textural Characterization

Nitrogen isotherms -196°C

Samples were outgassed at 120°C for 4 h, under vacuum of 10⁻⁶ bar before the experiment.



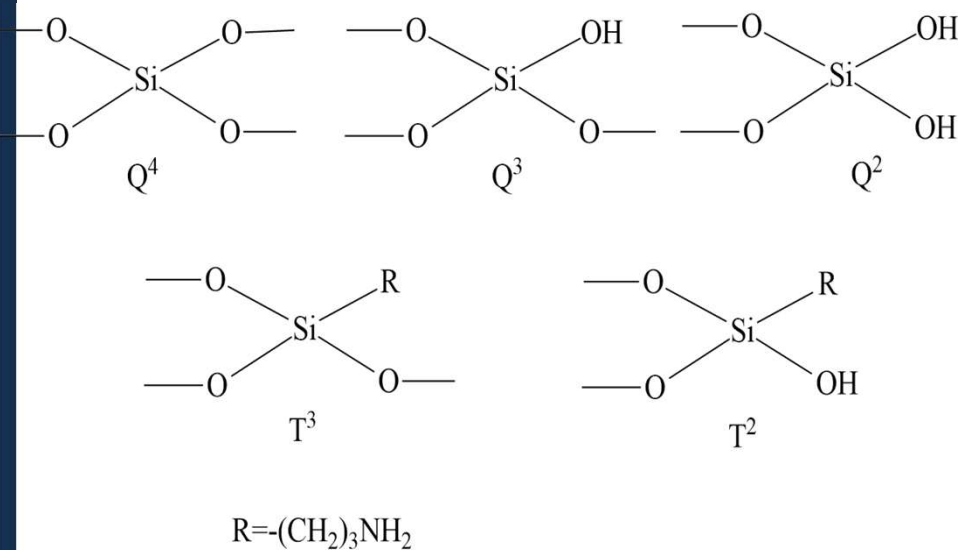
RESULTS AND DISCUSSION

Table 1 Textural properties calculated from N₂ isotherms and nitrogen content.

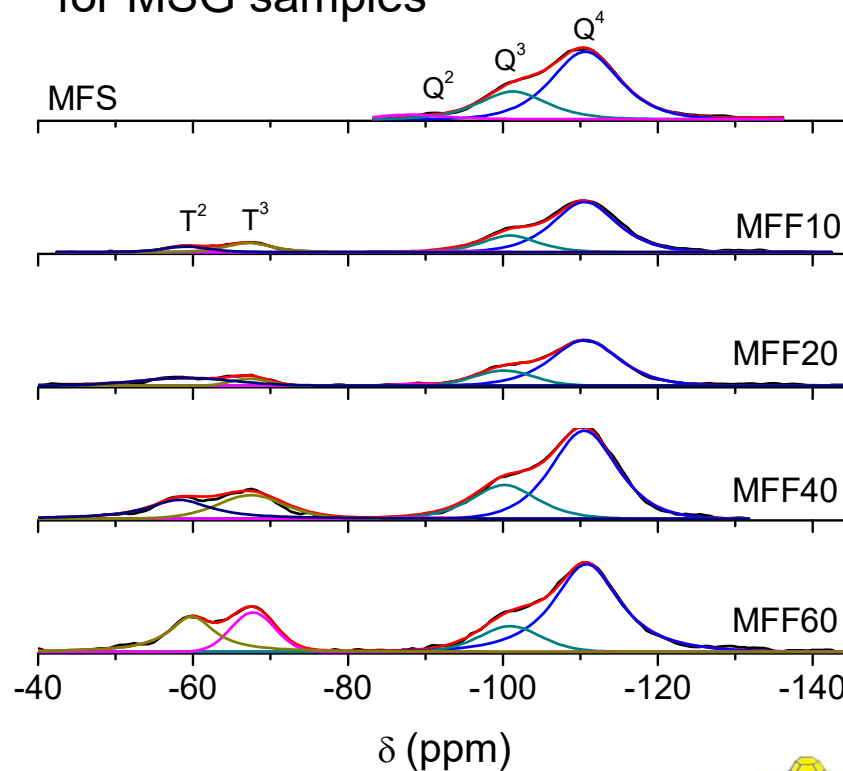
Samples	A _{BET} (m ² .g ⁻¹)	Pore Vol	Pore Size	Micro pore	N _C (mmol.g ⁻¹)
		(cm ³ .g ⁻¹)	(nm)	Vol (cm ³ .g ⁻¹)	
MFS	392	1.43	9.57	0.125	0.03
MFF10	213	1.02	7.81	0.057	1.57
MFF20	211	0.96	7.80	0.056	1.76
MFF40	215	0.98	7.80	0.056	1.95
MFF60	151	0.55	7.79	0.045	2.64

❖ Nuclear Magnetic Resonance (NMR ²⁹Si)

Chemical composition of chemical surface



Deconvolution ²⁹Si chemical shift signal for MSG samples



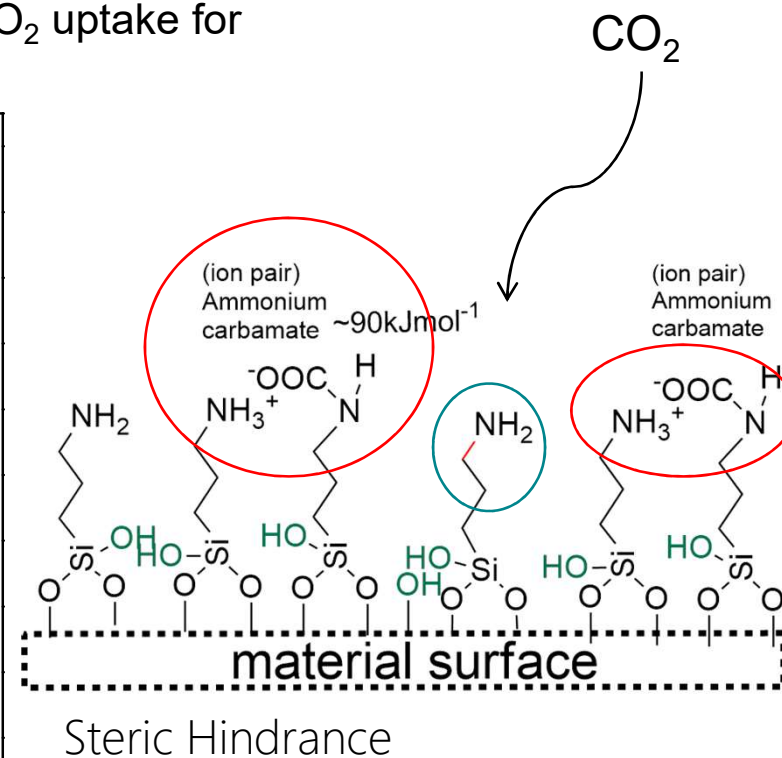
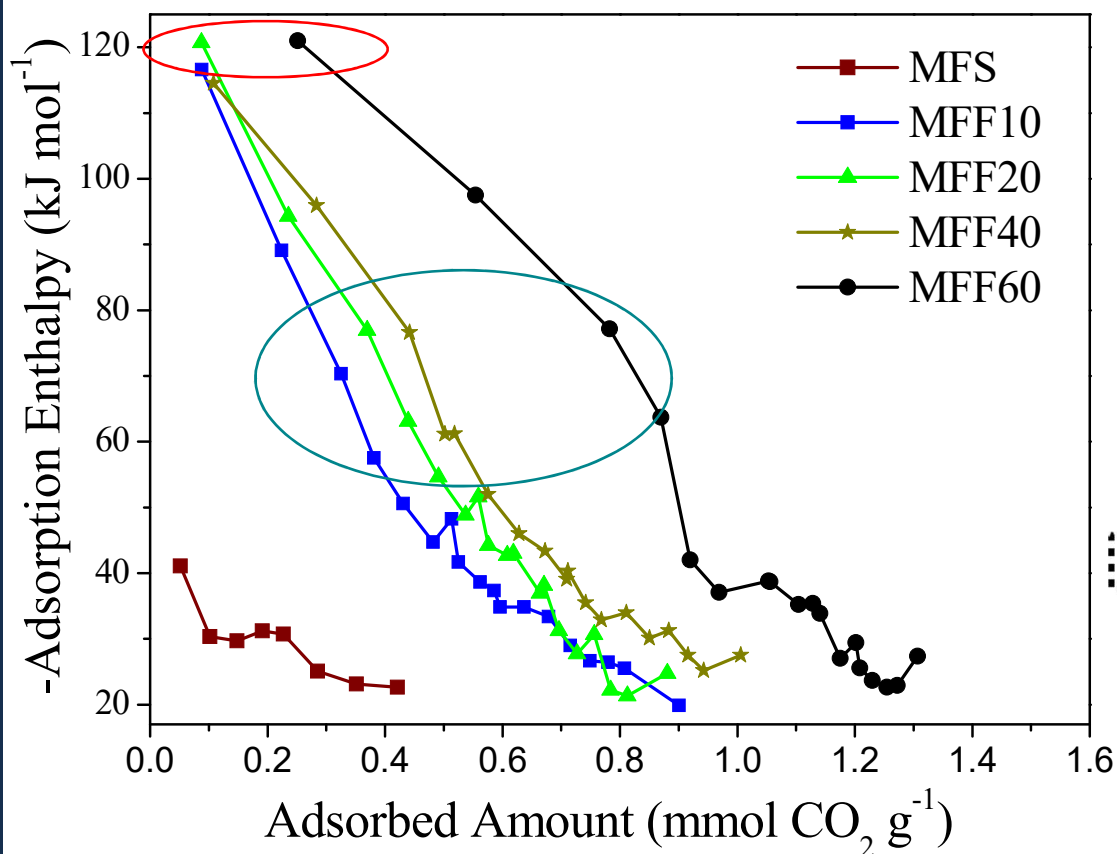
RESULTS AND DISCUSSION

Table ^{29}Si MAS NMR peak integration for mesoporous silica studied

Samples	T ² (int%)	T ³ (int%)	Q ² (int%)	Q ³ (int%)	Q ⁴ (int%)
MFS			3.8	28.0	68.2
MFF10	5.4	4.8	1.8	18.9	65.1
MFF20	11.2	8.8	1.2	17.0	62.7
MFF40	14.2	12.5	0.9	11.7	63.7
MFF60	20.0	12.2	—	6.7	61.2

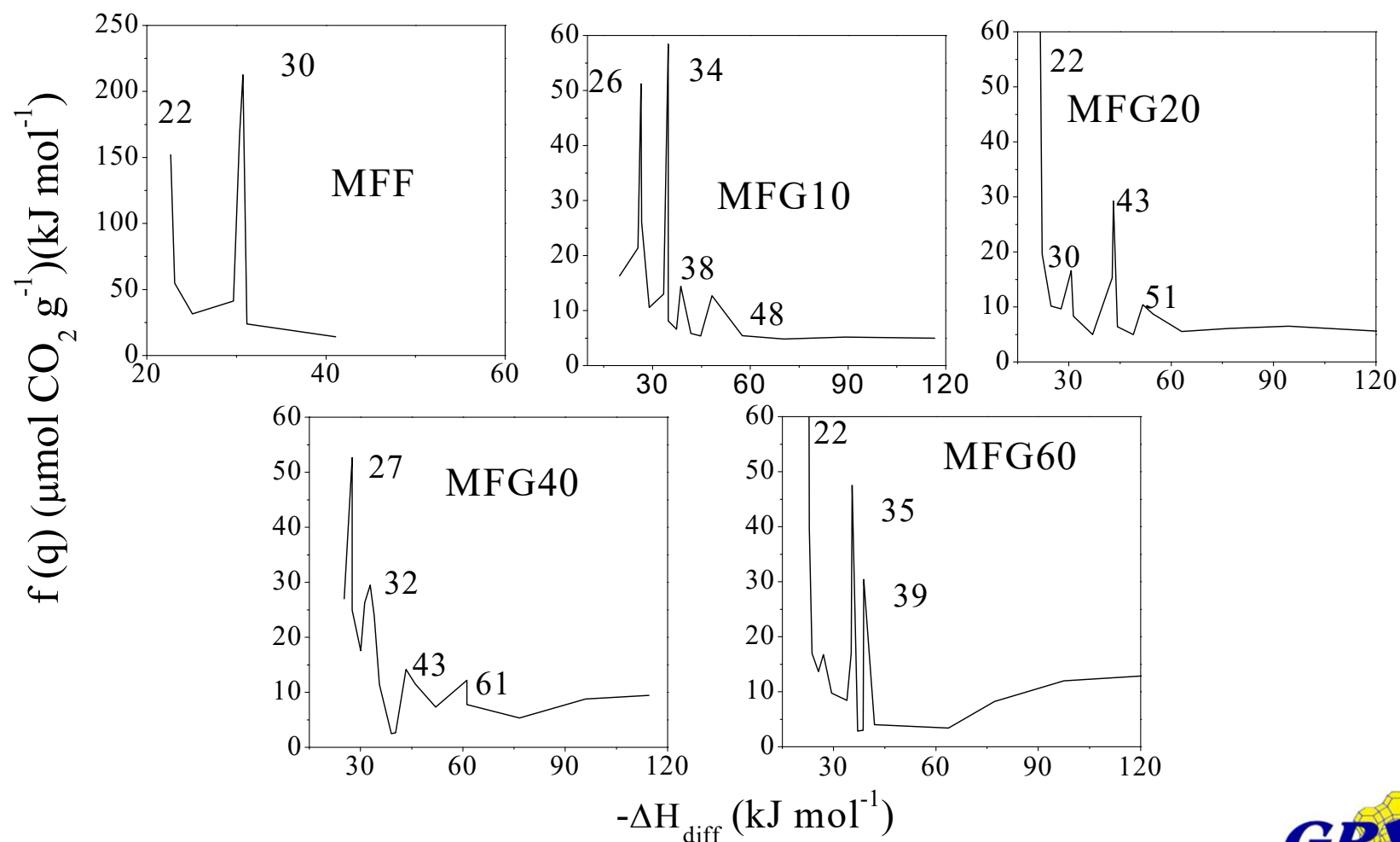
❖ Calorimetric Characterization

Differential enthalpy of adsorption in function of CO₂ uptake for mesoporous silica

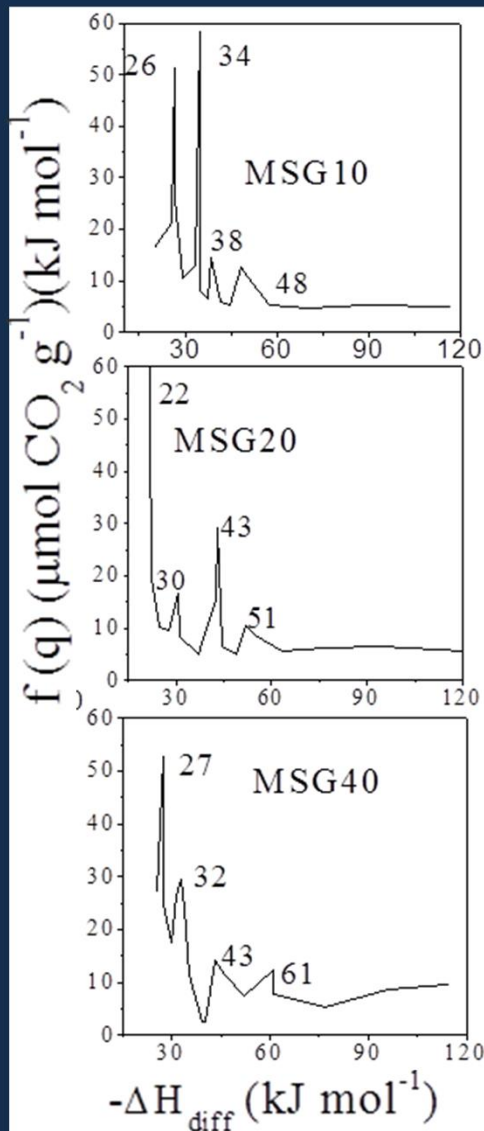


RESULTS AND DISCUSSION

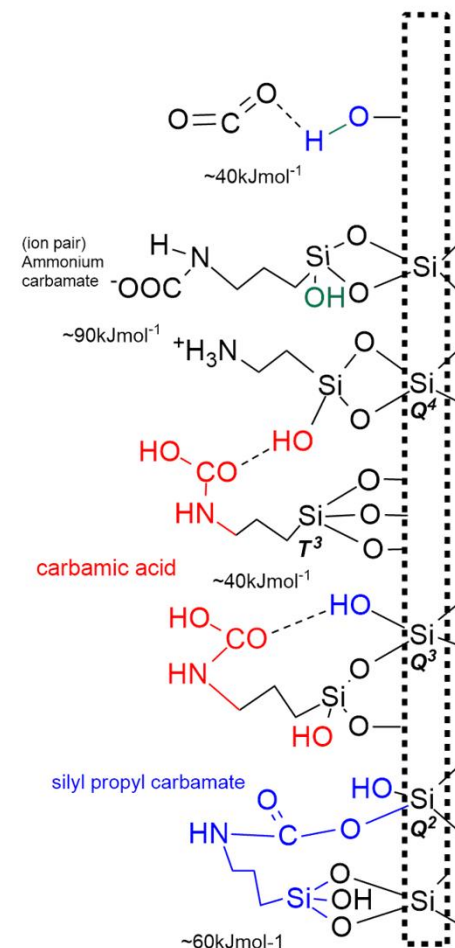
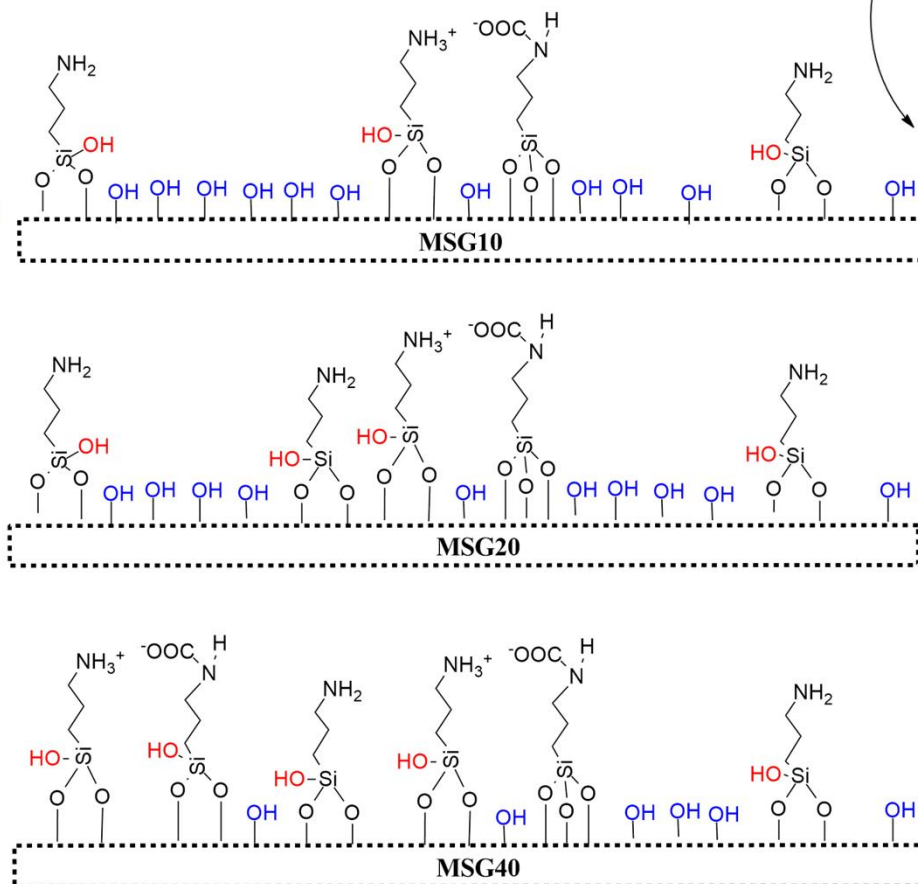
Energy site distribution



RESULTS AND DISCUSSION



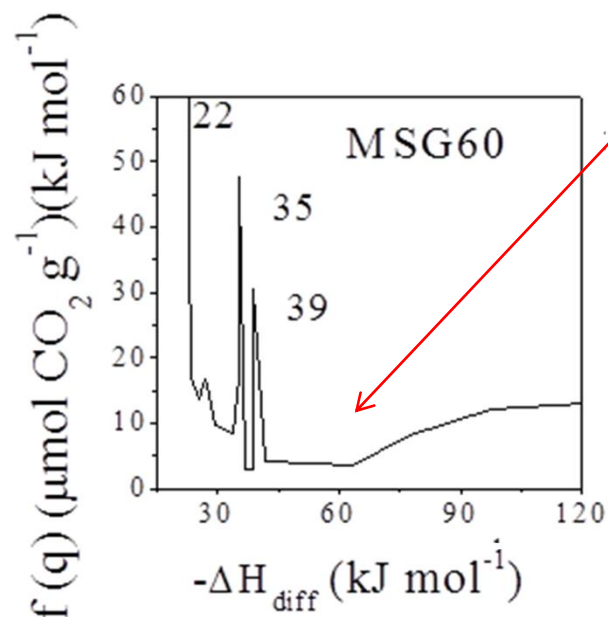
Hypothetical amine and silanols distribution based in the elemental analysis and NMR



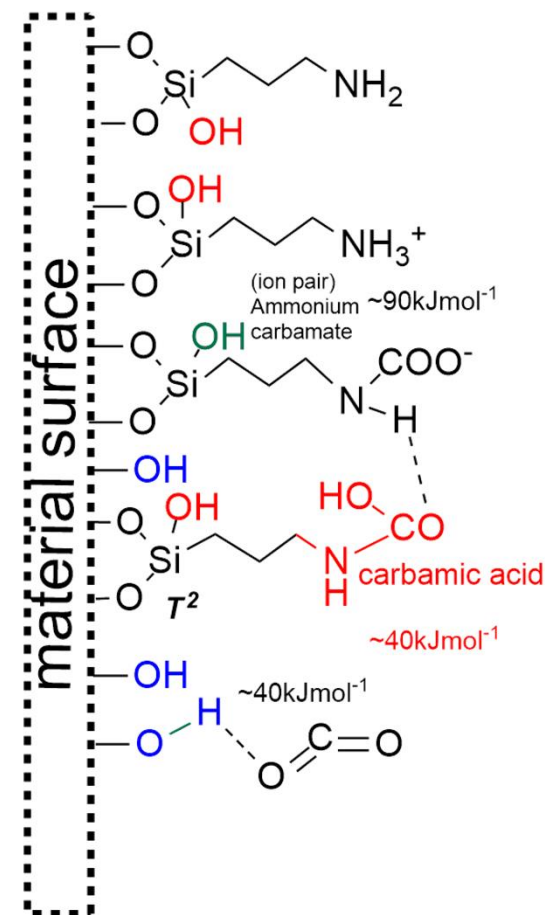
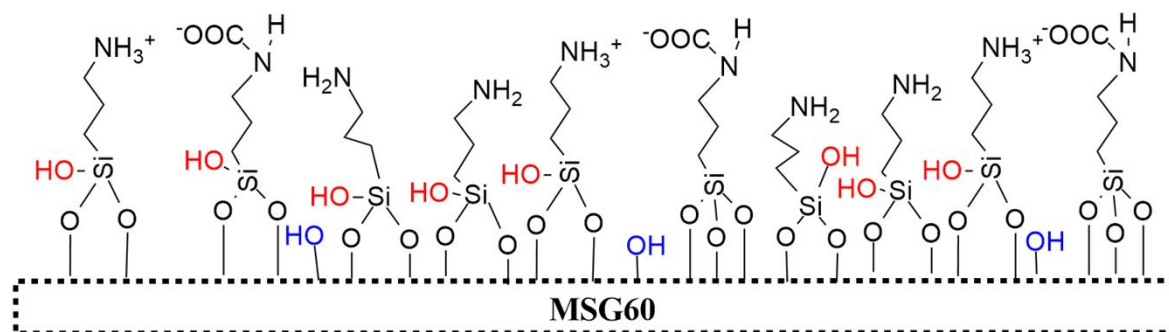
MEDIUM AMINE DENSITY

~4-5 molecules per nm²

RESULTS AND DISCUSSION



Silyl propyl carbamate was not formed on this sample



HIGH AMINE DENSITY

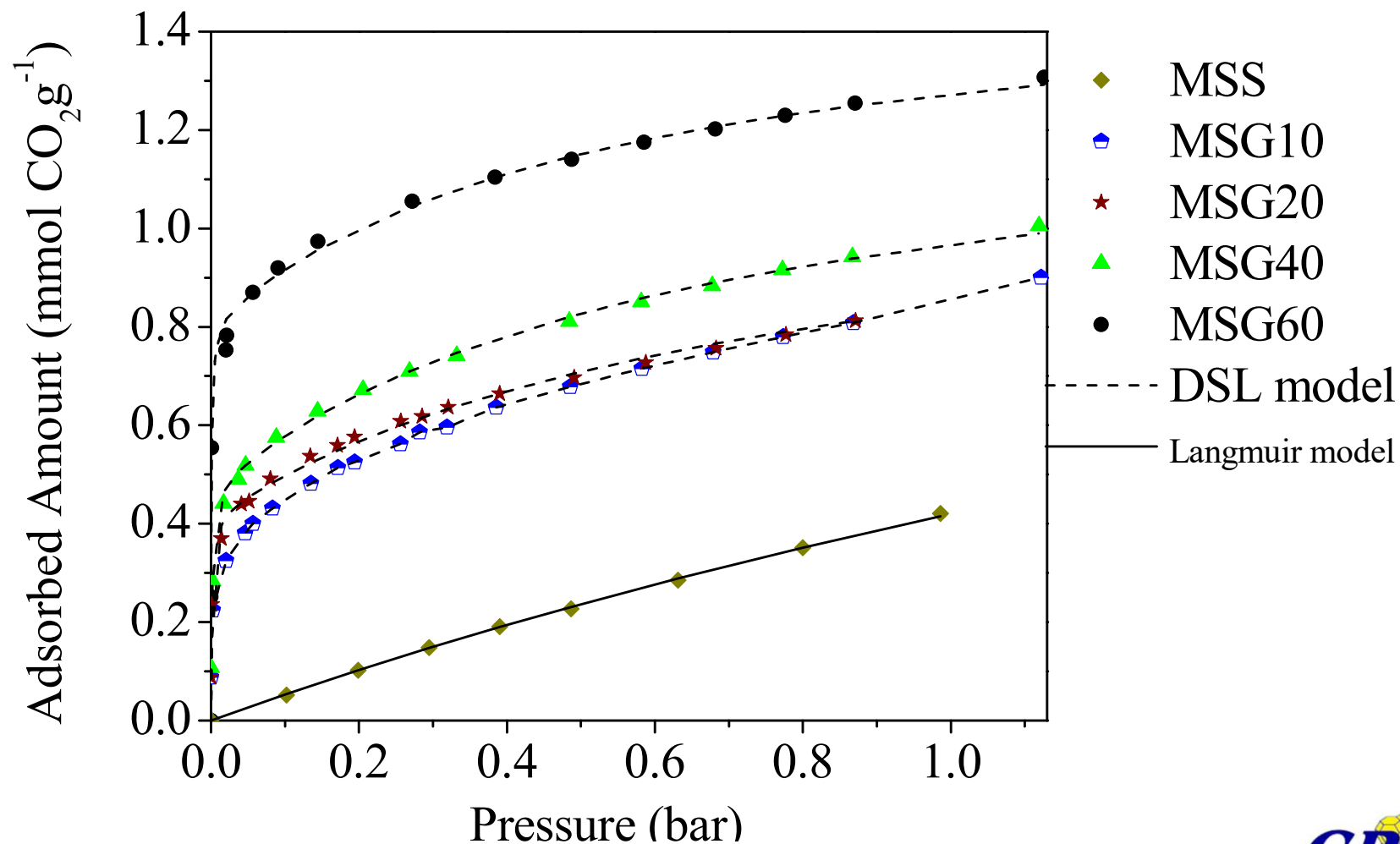
~ 10 molecules per nm^2

RESULTS AND DISCUSSION

Table 3. Maximum thermokinetic parameter ($\tau_{\max}$) and its corresponding enthalpy

Sample	$\emptyset_{\text{-NH}_2}$, Amine molecule. nm^{-2}	Maximum thermokinetic parameter ($\tau_{\max}$)	
		$\tau_{\max}$, s	ΔH_{ads} , kJ.mol^{-1}
MFS	-	397	30
MFF10	4.43	447	43
MFF20	5.02	354	43
MFF40	5.46	489	40
MFF60	10.53	613	64

❖ CO₂ isotherms at 25 °C for mesoporous materials





RESULTS AND DISCUSSION

Table 4 DSL fitting parameters to the experimental data at 25 ° C

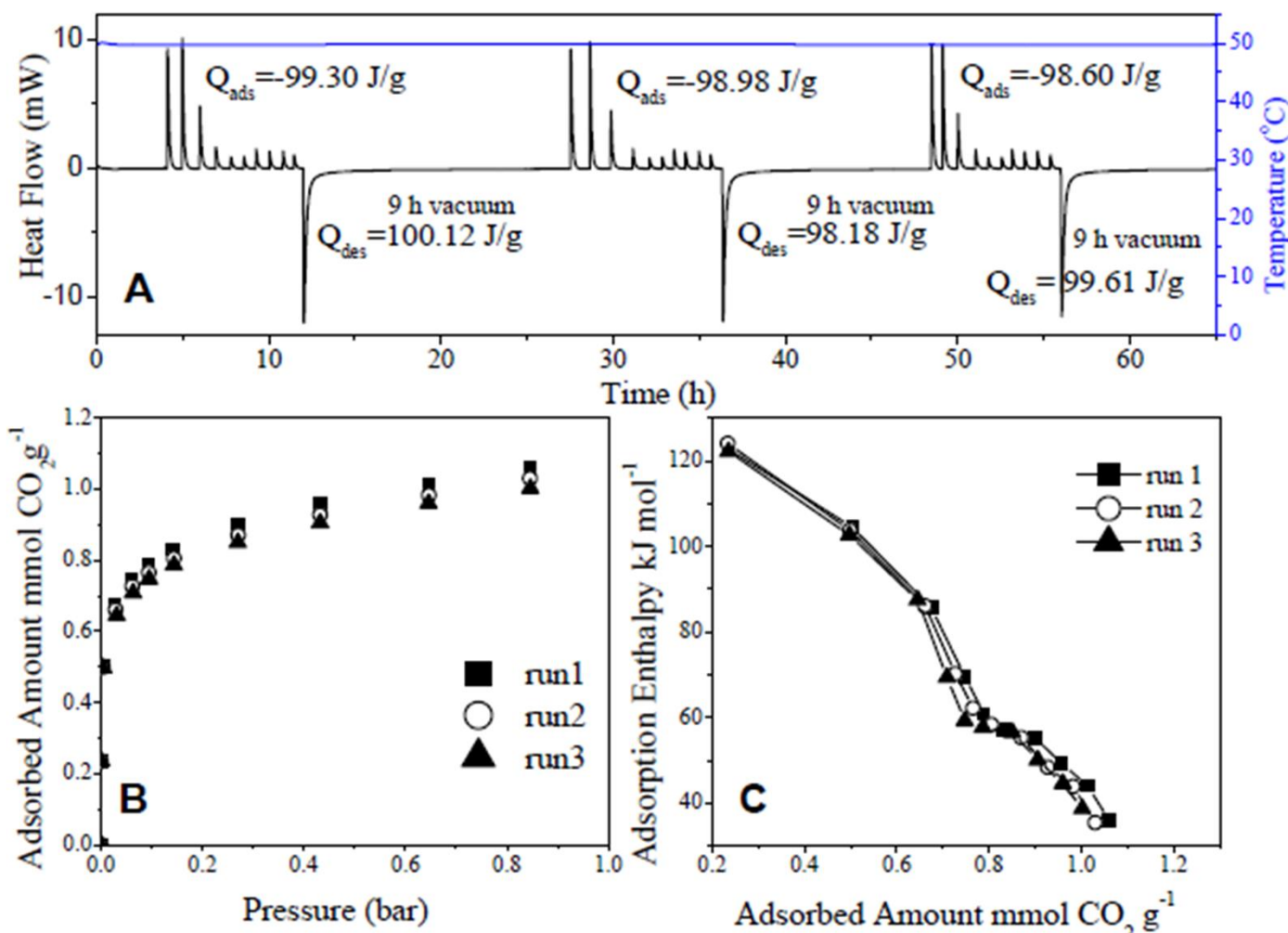
Parameter	MFS	MFF10	MFF20	MFF40	MFF60
$qm_1,$ $mmolCO_2g^{-1}$	0	0.34	0.42	0.47	0.79
b_1, bar^{-1}	0	671.1	795	823.7	2159
$qm_2,$ $mmolCO_2g^{-1}$	1.84	0.93	0.76	0.81	0.67
b_2, bar^{-1}	0.29	1.17	1.24	1.50	2.53
R^2	0.99	0.99	0.99	0.99	0.97



CONCLUSIONS

- This work aimed to understand how grafted amine density on silica supports having a direct impact on adsorbed CO₂ and on the strength of binding.
- The distribution of silanol groups was found to have key importance. Adsorption microcalorimetry together with ²⁹Si NMR and textural analysis were helpful tools to infer on CO₂ chemisorption products and the relative importance of physisorption.
- Thus we concluded that physisorption is the dominant binding mechanism for the support (MFS) whereas for MFF samples, in addition to physisorption, there is chemisorption leading to the formation of propyl ammonium carbamate, silyl propyl carbamate and propylcarbamic acid.
- The samples that present values of amine density around 5 molecules per nm² presented kinetic restrictions to stabilize carbamic acid as a product of CO₂ interaction with isolated amines. In contrast, functionalized materials having around 10 molecules per nm², the formation of silyl propyl carbamate is suppressed and acts as the limiting step to reach the equilibrium.
- Limited formation of silyl propyl carbamate may be advantageous because this species is irreversibly bound and cannot be removed only with vacuum.

Cycling adsorption-desorption for MFF60



Check oral presentation by Débora Maia (196) 24/04, 15:15



ACKNOWLEDGEMENTS



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LPACO2 team



Diana Azevedo

Full professor
H-index: 27
114 pubs
2038 citations
PQ-1C



Célio Cavalcante Jr.

Full professor
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121 pubs
1890 citations
PQ-1C



Eurico Torres

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536 citations



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373 citations
PQ-2



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124 citations

Post-Doc Fellows (02)



PhD Students (05)



MSc Students (03)



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